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Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- 1. (Currently amended) A process for the preparation and purification of protein(s) such as viral antigenic proteins, other recombinant therapeutic proteins, characterized in that the purification is carried out by a novel technique termed as using Hydrophobic Interaction Matrix (HIMAX) technology which is as herein described and recovering the said protein (s). comprising:
- (a) lysing, in the absence of a detergent, vector cells expressing said protein(s) to obtain a cell lysate;
- (b) centrifuging the cell lysate between 1000g and 10,000g to form a supernatant portion and solid portion:
- (c) obtaining the solid portion from step (b) wherein the solid portion comprises the protein(s);
 - (d) suspending the solid portion in a buffer of pH 6 to 7.5;
- (e) forming an insoluble matrix after step (d) by the addition of divalent ionic salt having a concentration ranging from 0.2% to 10% with counter ions of either phosphate, chloride and/or acetate solution to the suspension;
 - (f) subjecting the insoluble matrix to centrifugation optimally to form a pellet;
- (g) subjecting the pellet from step (f) to a repeated desorption process to release the protein(s) from said insoluble pellet by using either Tris buffer of pH 8. 0 to 8.5 or Tris buffer with EDTA at pH 7.0 to 8.0; and
 - (h) recovering the protein(s) through hydrophobic chromatography.

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- 2. (Currently amended) The process as claimed in of claim 1 wherein [[the]] said protein(s) is/are made to be expressed in the vectors like prokaryotic cell or cukaryotic cell like E.Coli, yeast-etc.
- 3. (Currently amended) [[The]] A process as elaimed in the preceding claims wherein the said process for the preparation and purification of protein(s) by using Hydrophobic Interaction Matrix (HIMAX) technology comprising comprising:
- (a) [[the]] <u>lysing vector cells expressing said protein(s)</u> are subjected to lysis in the absence of a detergent to obtain a cell lysate;
- (b) subjecting the cell lysate of steps as to centrifugation ranging from 1000g to 10,000g;
- (c) obtaining a solid pellet portion from step (b) by decantation wherein the said solid pellet portion comprising comprises [[the]] said proteins;
- (d) suspending the said solid pellet portion in a buffer of pH 6 to 7.5 having divalent ions ranging from 0.2% to 10% and counter ions of either phosphate, chloride and/or acetate optimally treating this with wherein a detergent is not used such as herein described to solubulize the minute impurities if any; and

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- 4. (Currently amended) The process as claimed in any of the preceding claims of claim 2, wherein [[the]] said protein is a viral antigen.
- 5. (Currently amended) The process as claimed in of claim 4 wherein inactivation of the viral antigens is carried out by a known manner antigen is inactivated before said subjecting to desorption (by chromatography) step process.
- 6. (Currently amended) The process as claimed in claims 1 to 3 of claim 5, wherein [[the]] said protein is one other than a viral antigen.
- 7. (Currently amended) The process as claimed in of claim 6 wherein said inactivation step is avoided before desorption.
- 8. (Currently amended) The process as claimed in the preceding claims of claim
 7. wherein the chromotographically purified fractions containing the desired protein(s) are pooled for diafiltration and or and/or for sterile filtration.
- 9. (Currently amended) The process as claimed in the preceding claims of claim 8, wherein the divalent ionic salt is a salt of divalent cations is preferably Zh cation Zn, ea Ca, or Mg, or a combination thereof.
- 10. (Withdrawn) The process as claimed in step (d) of claim 3 wherein the detergent is non-ionic detergent.
- 11. (Currently amended) The process as claimed in step (d) of claim 3, wherein the detergent is not used for the preparation and purification of protein(s).
- 12. (Withdrawn) The process as claimed in step (h) of claim 3 wherein ultra filtration is carried out using membrane filters of 100-300K molecular weight cut off.

- 13. (Withdrawn) The process as claimed in step (h) of claim 3 wherein the ion-exchange matrices is selected from anionic exchange resins such as sulphated cellulose/DEAE matrices.
- 14. (Currently amended) The process as claimed in the preceding claims of claim 8, wherein the said proteins are highly purified without the loss of biological activity.
- 15. (Currently amended) The process as claimed in <u>any of</u> the preceding claims wherein the contaminants like nucleic acid-fragments etc.; does do not interfere with/affect the [[said]] process of preparation and purification of [[the]] said proteins.
- 16. (Currently amended) The process as claimed in any-of the preceding claims of claim 2, wherein said proteins are viral antigens, recombinant proteins, and/or biotherapeutic proteins etc., are simultaneously prepared and purified.
- 17. (New) The process of claim 16, wherein said proteins are simultaneously prepared and purified.
- 18. (New) The process of claim 16, wherein said proteins are selected from the group consisting of: Rabies antigen, Hepatitis A antigen, Diptheria toxoid and Tetanus toxoid.